

### **IN THE SPECIFICATION:**

At the bottom of page 4, please insert the following paragraphs:

-- Fig. 3 illustrates a coldbox, indicated with reference number 11, with two heat exchanger blocks (1) hanging on a double-T support (8) which is fixed within the coldbox (11).

Fig. 4 is a top view of a coldbox (11) enclosing six heat exchanger blocks (1) which are hanging on three double-T supports (8). The figure shows a discharge pipeline connected to the cold end of each heat exchanger block (1) with all discharge pipelines leading to one common connection line (reference number 12).

Fig. 5 illustrates a heat exchanger block (1) which is directly fixed to the coldbox (11) without using a double-T support (8).

Fig 6 is similar to Fig. 4 and illustrates a top view of a coldbox (11) enclosing ten heat exchanger blocks (1) in two rows.

Fig. 7 illustrates a fractionation plant comprising a fractionation column (16) and a principal heat exchanger (15). --

Please AMEND the paragraph beginning at page 5, line 6, with the following:

The heat exchanger block 1 is up to 240 cm wide. A connector/distributor 2, known as a header, is arranged on the heat-exchanger block 1, from which header one or more pipelines (~~not shown~~) 13 lead away.

Please AMEND the paragraph beginning at page 5, line 22 with the following:

At the third corner of the steel plate 4 there is a further joint 7. The steel plate 4 is suspended by means of the joint 7 from a double-T support 8, which is secured in the coldbox (~~not shown~~) 11 (Figs. 3-6) and supports the heat exchanger block 1. The joint 7 allows movement

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in the plane of the steel plate 4 or about an axis 9 perpendicular to the steel plate 4. --

Please delete page 5a.

Please AMEND the paragraph beginning at page 6, line 9 with the following:

One or more pipelines (~~not shown~~) for supplying 14 and discharging 12 the fluid streams which are to be brought into heat exchange with one another are arranged at the lower end of the heat exchanger block 1. In the event of load changes and when the plant is being heated and cooled down, these pipelines undergo changes in length of approximately 3 to 4 mm per meter of pipeline length, for thermal reasons. The fact that, according to the invention, the heat exchanger block 1 is suspended above its center of gravity means that it is moved by even relatively minor forces acting on its lower end. The movement of the heat exchanger block 1 compensates for the thermally induced changes in pipe length, so that there is no need for pipe loops for compensating for contraction in the pipelines.--